A CFD Investigation of Flows through an Artificially Roughened Solar Air Heater

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Abstract- Solar air heaters, because of their simple in design, is cheap and most widely used collection devices of solar energy. The thermal efficiency of a solar air heater is significantly low because of the low value of the convective heat transfer coefficient between the absorber plate and the air, leading to high absorber plate temperature and high heat losses to the surroundings. This paper presents the study of heat transfer in a solar air heater by using Computational Fluid Dynamics (CFD). The effect of Reynolds number on Nusselt number is investigated. A commercial finite volume package ANSYS FLUENT 16 is used to analyze and visualize the nature of the flow across the duct of a solar air heater.

Keywords- Solar Air Heater, Heat transfer, Pressure Drop, CFD.

I. INTRODUCTION

Solar air heater is one of the basic equipment through which solar energy is converted into thermal energy. Solar air heaters, because of their simple in design, are cheap and most widely used collection devices of solar energy. The main application of solar air heaters is space heating, seasoning of timber, curing of industrial products and these can also be effectively used for curing/drying of concrete/clay building components.

A conventional solar air heater generally consists of an absorber plate, a rear plate, insulation below the rear plate, transparent cover on the exposed side, and the air flows between the absorbing plate and rear plate. A solar air heater is simple in design and requires little maintenance. However, the value of the heat transfer coefficient between the absorber plate and air is low and this results in a lower efficiency. For this reason, the surfaces are sometimes roughened in the air flow passage.

The concept of artificial roughness was first applied by Joule [1] to enhance heat transfer coefficients for in-tube condensation of steam and since then many experimental investigations were carried out on the application of artificial roughness in the areas of cooling of gas turbine, electronic equipments, nuclear reactors, and compact heat exchangers etc. Nunner [2] was the first who developed a flow model and likened this model to the temperature profile in smooth tube flow at increased Prandtl number.

The proposed flow model predicts that roughness reduces the thermal resistance of the turbulence dominated wall region without significantly affecting the viscous region. The argument was quantified by using the Prandtl analogy and replacing Pr by (f/fs)Pr. This model predicts that value of St/Sts decreases with increase in Prandtl number. The proposed flow model also predicts that St/Sts, is independent of the roughness type. A friction correlation for flow over sand-grain roughness was developed by Nikuradse [3].

Based on law of the wall similarity, Nikuradse presented the pressure drop results in terms of roughness function R and roughness Reynolds number e+.

Dipprey and Sabersky [4] developed a heatmomentum transfer analogy relation for flow in a sand-grain roughened tube and achieved excellent correlation of their data. The concept proposed by Dipprey and Sabersky was so common and it can be applied to any roughness for which law of the wall similarity holds. Prasad and Mullick [5] were the first

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who introduced the application of artificial roughness in the form of small diameter wire attached on the underside of absorber plate to improve the thermal performance of solar air heater for drying purposes.

After Prasad and Mullick's [5] work a number of experimental investigations of solar air heater involving roughness elements of different shapes, sizes and orientations with respect to flow direction have been carried out in order to obtain an optimum arrangement of roughness element geometry [6-7].

Chaube et al. [8] conducted a CFD based analysis of heat transfer and fluid flow characteristics of an artificially roughened solar air heater. Kumar and Saini [9] performed a CFD analysis of fluid flow and heat transfer characteristics of a solar air heaters having arc shaped artificial roughness on the absorber plate.

Karmare and Tikekar [10] carried out CFD investigation of fluid flow and heat transfer in a solar air heater duct with metal grit ribs as roughness elements on the absorber plate. Yadav and Bhagoria [11] conducted a numerical prediction to study only heat transfer behavior of a rectangular duct of a solar air heater having triangular rib roughness on the absorber plate.

Yadav and Bhagoria [12] presented the numerical prediction of fluid flow and heat transfer in a conventional solar air heater by CFD. A commercial finite volume package ANSYS FLUENT 12.1 was used to analyze the nature of the flow across the duct of a conventional solar air heater. Yadav and Bhagoria [13-14] presented a detailed literature survey about different CFD investigations on artificially roughened solar air heater. Several other types of turbulators elements were used extensively to improve the heat transfer characteristics [15-69].

The aim of present study is to analyze CFD investigation of ribbed rectangular channel on the flow and heat transfer.

The aim of our study is to improve the prediction of the flow in the solar air heater. A near-wall function for TKE will be implemented in Computational Fluid Dynamics code Fluent. Second order upwind and SIMPLE algorithm were used to discretize the governing equations. The FLUENT software solves the following mathematical equations which governs fluid flow, heat transfer and related phenomena for a given physical problem.

II. CFD MODELING AND ANALYSIS

Computational Fluid Dynamics (CFD) is the science of determining numerical solution of governing equation for the fluid flow whilst advancing the solution through space or time to obtain a numerical description of the complete flow field of interest.

The equation can represent steady or unsteady, Compressible or Incompressible, and in viscid or viscous flows, including non-ideal and reacting fluid behavior. The particular form chosen depends on intended application. The state of the art is characterized by the complexity of the geometry, the flow physics, and the computing time required obtaining a solution.

The 2-D computational domain used for CFD analysis having the height (H) of 20 mm and width (W) 100 mm as shown in Fig. 1. In the present analysis, a 2dimensional computational domain of artificially roughened solar air heater has been adopted which is similar to computational domain of Yadav and Bhagoria [14].



Fig 1. 2-D computational domain.

After defining the computational domain, nonuniform mesh is generated. In creating this mesh, it is desirable to have more cells near the plate because we want to resolve the turbulent boundary layer, which is very thin compared to the height of the flow field. After generating mesh, boundary conditions have been specified. We will first specify that the left edge is the duct inlet and right edge is the duct outlet. Top edge is top surface and bottom edges are inlet length, outlet length and solar plate.

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All internal edges of rectangle 2D duct are defined as turbulator wall. Meshing of the domain is done using ANSYS ICEM CFD V16 software. Since low-Reynoldsnumber turbulence models are employed, the grids are generated so as to be very fine.

Present non-uniform quadrilateral mesh contained 161,568 quad cells with non-uniform quad grid of 0.22 mm cell size. This size is suitable to resolve the laminar sub-layer. For grid independence test, the number of cells is varied from 103,231 to 197,977 in five steps. It is found that after 161,568 cells, further increase in cells has less than 1% variation in Nusselt number and friction factor value which is taken as criterion for grid independence.

To select the turbulence model, the previous experimental study is simulated using different low Reynolds number models such as Standard k- ω model, Renormalization-group k ϵ model, Realizable k ϵ model and Shear stress transport k- ω model. The results of different models are compared with experimental results. The RNG k- ϵ model is selected on the basis of its closer results to the experimental results. The working fluid, air is assumed to be incompressible for the operating range of duct since variation is very less.

The mean inlet velocity of the flow was calculated using Reynolds number. Velocity boundary condition has been considered as inlet boundary condition and outflow at outlet. Second order upwind and SIMPLE algorithm were used to discretize the governing equations. The FLUENT software solves the following mathematical equations which governs fluid flow, heat transfer and related phenomena for a given physical problem.

III. RESULTS AND DISCUSSIONS

Results are presented in form of graphs, representing the average Nusselt number at different Reynolds numbers, and in form of temperature and velocity contours at particular sections for a fixed Reynolds number.

Fig. 2 shows the effect of Reynolds number on average Nusselt number for different values of relative roughness height (e/D) and fixed value of pitch. The average Nusselt number is observed to increase with increase of Reynolds number due to the increase in turbulence intensity caused by increase in turbulence kinetic energy and turbulence dissipation rate.

The roughened duct with relative roughness height of 0.06 provides the highest Nusselt number at a Reynolds number of 18000. The roughened duct with relative roughness height (e/d) of 0.015 provides the lowest Nusselt number at a Reynolds number of 3800. The maximum enhancement of average Nusselt number is found to be 2.78 times that of smooth duct for relative roughness height of 0.06.



Fig 2. Variation in Nusselt number.

The heat transfer phenomenon can be observed and described by the contour plot of turbulence intensity. The intensities of turbulence are reduced at the flow field near the rib and wall and a high turbulence intensity region is found between the adjacent ribs close to the main flow which yields the strong influence of turbulence intensity on heat transfer enhancement.

Fig 3 shows that the friction factor decreases with the increasing values of the Reynolds number in all cases as expected because of the suppression of laminar sub-layer for fully developed turbulent flow in the duct.

The maximum and minimum value of friction factor occurs at relative roughness height (e/d) of 0.06 and 0.015 respectively for the range of parameters investigated. It is also observed that the maximum enhancement of average friction factor is found to be 4.24 times that of smooth duct for relative roughness height of 0.06 at a Reynolds number of 3800.

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Fig 3. Variation in Friction factor.

The fluid friction phenomenon can be observed and described by the contour of pressure for circular rib. The contour plot of pressure is shown in Fig. 4. Similar pattern is obtained for contour plot of pressure for semi-circular rib. The flow friction phenomenon can be observed and described by the contour plot of pressure for semi-circular rib.



Fig 4. Contour plot.

In order to validate the present numerical model, the results are compared with available experimental results. Literature search in the area of artificially roughened solar air heater also reveal that the optimum value of relative roughness height generally lies between 0.03-0.047.

The comparison of optimum value of relative roughness height between present CFD simulation and available experimental/widely accepted numerical results. On comparison, it has been observed that the optimum value of relative roughness height for present CFD model is found to be 0.045 for circular and semi-circular sectioned rib.

The optimum value of relative roughness height from present CFD investigation is found to fall in-between the accepted range i.e. 0.033 and 0.043. It can be seen that there is a good agreement between CFD and experimental/numerical results.

IV. CONCLUSION

The effect of relative roughness pitch and Reynolds number on the heat transfer coefficient and friction factor have been studied. CFD Investigation has been carried out in medium Reynolds number flow (Re = 3800–18,000).

Based on the CFD investigations of heat and fluid flow in a rectangular duct with protrusions as roughness element on one broad wall subjected to a uniform heat flux the following conclusions were drawn:

- Average Nusselt number increases with an increase of Reynolds number. The maximum value of average Nusselt number is found at relative roughness height of 0.06 at a higher Reynolds number, 18,000.
- Average friction factor decreases with an increase of Reynolds number. The maximum value of average friction factor is found at relative roughness height of 0.06 at a lower Reynolds number, 3800.
- The Renormalization-group (RNG) k-ε turbulence model predicted very close results to the experimental results, which yields confidence in the predictions done by CFD analysis in the present study. RNG k-ε turbulence model has been validated for smooth duct and grid independence test has also been conducted to check the variation with increasing number of cells.
- The discrepancy between available experimental data and present computational results is less than ±10%. It can therefore be concluded that the present computational results are reasonably satisfactory.

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